IS 9522 (1980): Code of practice for agitator equipment
[MED 17: Chemical Engineering Plants and Related Equipment]

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(Reaffirmed 2006)

Indian Standard

CODE OF PRACTICE FOR AGITATOR EQUIPMENT

Chemical Engineering Sectional Committee, EDC 57; Process Vessels Subcommittee, EDC 57 : 2 [Ref : Doc : EDC 57 (3173)]

1. Scope — Lays down the standard recommended capacities of agitator equipment and general requirements of agitator equipment. It also provides guidelines on the selection of impeller, power assessment, drive and bearing arrangements and shaft design.

2. Nomenclature — For the purpose of this standard the different parts of agitator equipment shall be designated as given in the following table. They are numbered for identification in Fig. 1.

1.	Shell	15.	Gear box
2.	Shell cover	16.	Motor
3.	Vessel flange	17.	Draft tube
4.	Agitator shaft	18.	Baffles
5.	Impeller	19.	Mechanical seal
6.	Impeller hub	20.	Lantern ring
7.	Rigid coupling	21.	Bearing housing
8.	Flexible coupling	22.	Sparger pipe
9.	Stuffing box	23.	Headers
10.	Stuffing gland	24.	Jacket
11.	Packing	25.	Heating coil
12.	Thrust bearing	26.	Half tubes (limpet coils)
13.	Roller bearing	27.	Manhole
14.	Drive, mounting	28.	Vessel supports

3. Terminology — For the purpose of this standard the following definitions shall apply.

3.1 *Agitator* — The assembly consisting of impeller, impeller shaft and drive including other parts such as gland, and bearing used in conjunction with the above.

3.2 *Impeller* — The actual element which imparts movement to the charge (fluid).

3.3 *Propeller* — A high speed impeller which essentially imparts axial thrust to the fluid.

3.4 *Turbine* — An impeller with essentially constant blade angle with respect to a vertical plane, over its entire length or over finite sections, having blades either vertical or set at an angle less than 90° with the vertical.

3.5 *Paddle* — An impeller with four or fewer blades, horizontal or vertical, and essentially having a high impeller to vessel diameter ratio.

3.6 *Anchor* — Basically a paddle type impeller which is profiled to sweep the wall of the containing vessel with a small clearance.

3.7 *Baffle* — An element fixed inside the vessel to impede swirl.

3.8 *Draught Tube* — A tubular fitting which is arranged to direct the liquid flow produced by the impeller.

3.9 *Filling Ratio* — The ratio of liquid depth in the vessel to vessel diameter.

3.10 *Swirling* — The continuous rotation of liquid about a fixed axis.

3.11 *Vortex* — A depression in the surface of a liquid produced by swirling.

3.12 *Fully Baffled Condition* — A condition when any further increase in baffling causes no significant increase in power consumption; this may be considered as a state where the liquid swirl in the vessel has become negligibly small and when all the power input to the impeller expended to create turbulence.

4. Recommended Capacities and Vessel Sizes — The capacities and the corresponding vessel diameters are shown in Table 1. The vessel diameter shown against each capacity are selected so as to obtain an approximate filling ratio of 1·0 for vessels with torispherical bottom ends. However, depending on the filling ratio requirement for a specific application and other process considerations, the vessel diameters may be suitably selected.

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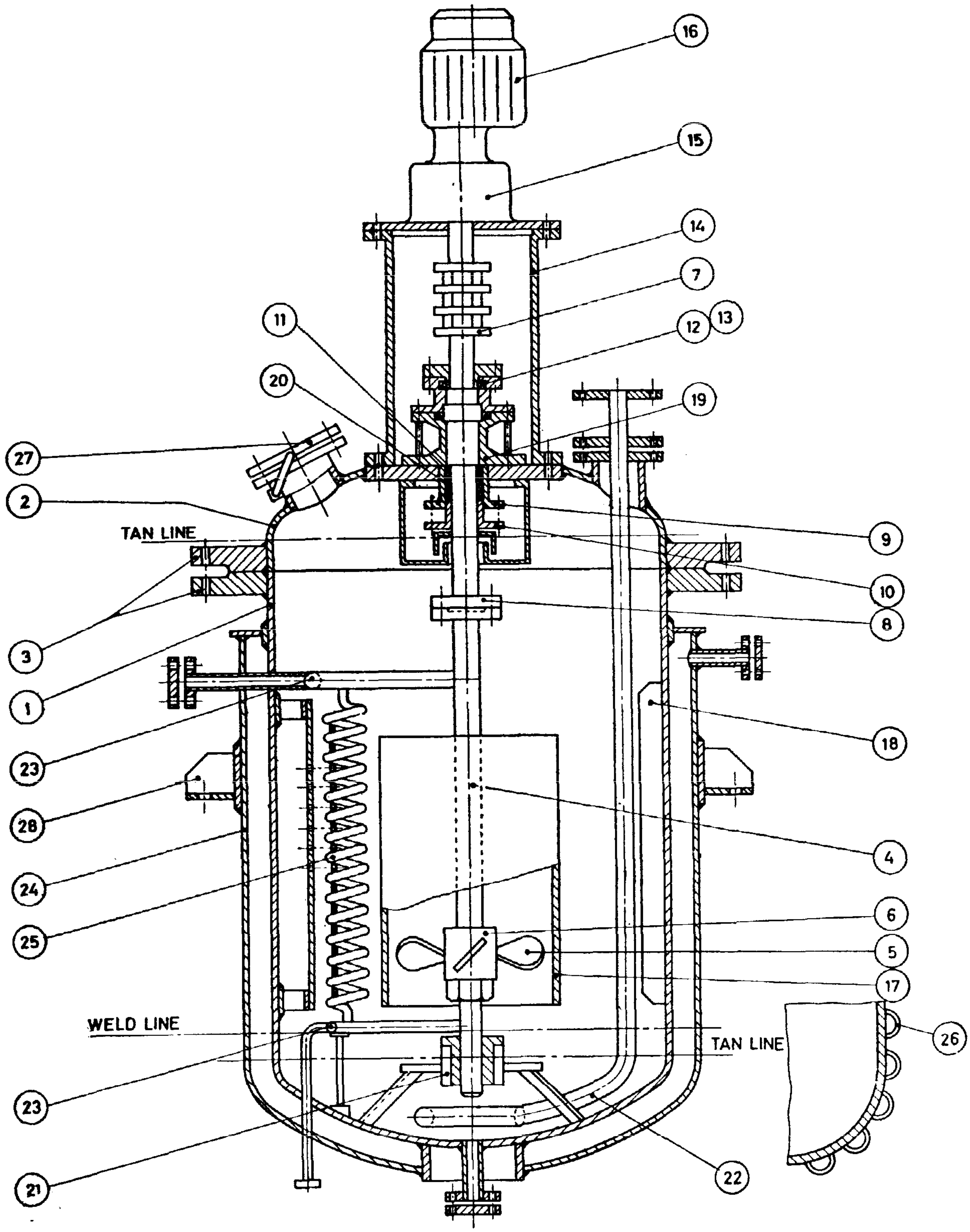


FIG. 1 AGITATOR ASSEMBLY

5. General Requirements of Mixing Equipment — The general requirements of the mixing equipment given below mainly relate to vertical vessels only.

TABLE 1 CAPACITIES AND VESSEL DIAMETERS

(*Clause* 4)

Nominal Capacity Litres	Vessel Outside Diameter mm
(1)	(2)
250	700
400	800
630	1 000
(750)	1 000
1 000	1 200
(1 250)	(1 300)
1 600	1 400
(2 000)	(1 500)
2 500	1 600
(3 200)	(1 700)
4 000	1 800
(5 000)	(2 000)
6 300	2 100
(8 000)	(2 300)
10 000	2 400

Note — Values given in the brackets are second preference values.

5.1 *Filling Ratio* — Filling ratio normally varies between 0·5 and 1·5 and a value approximately equal to 1·0 is suitable for most of the applications. However, in some applications like dispersing gas in a liquid, a filling ratio of about 2·0 may be sometimes necessary in order to maintain a sufficiently long period of contact between gas and liquid. Normally for the same agitating effect, the power consumption per unit volume increases as the filling ratio departs from unity.

5.2 *Shape of the Vessel* — Vertical cylindrical vessels with dished bottoms are usually chosen for the mixing operation but use of cylindrical vessels with flat or shallow coned-bottoms is not uncommon. The significance of the bottom shape of the vessel increases as the filling ratio reduces, and other things being equal vessels with dished bottoms tend to be economical in power consumption. The flat bottomed and cone-bottomed vessels have the disadvantage of low agitation efficiency in the corner formed between the wall and flat bottom in the former case and in the apex of the cone bottom in the latter case. In mixing applications like suspension of heavy solids in a liquid, the presence of the low agitation efficiency areas allows the settlement of the solids which is detrimental to the process requirements. In such cases, fillets should be inserted in the corners and in the apex to avoid the low agitation areas.

5.3 *Roughness of Vessel Walls* — Power consumption will be more in a rough walled vessel than a smooth walled vessel due to the increase in local turbulence at the walls. Even if the turbulence is the primary objective of the agitator, the local increase in turbulence at the walls is of little value and an increase in turbulence when definitely required is best achieved by baffles. Hence vessel walls should be as smooth as possible.

5.4 *Baffles* — In applications where turbulence is primary requisite, the baffles are used to promote turbulence. Baffles also allow the system to absorb relatively large amount of power where it is needed for effective mixing, avoiding vortex and swirling action. Four numbers of baffles are sufficient to achieve a fully baffled condition for vessels of diameter up to 2 500 mm and above which six number may be necessary. Baffles are straight flats and normally of width one-tenth of the vessel diameter. However, when the baffles are used in conjunction with a heating coil inside the vessel, the baffle width may be reduced to one-twelfth of the vessel diameter. The baffles should be mounted vertically and radially in a vessel at equal spacings leaving a clearance of one-third to one-fourth of the baffle width between the vessel walls and baffles to reduce and tendency for solid deposits to form in the corners between vessel wall and baffles and to facilitate cleaning of the vessel. Baffles should normally extend up to liquid surface with a small clearance at the bottom end between baffles and flat bottomed ends.

5.5 *Draft Tube* — The draft tube is a tubular fitting surrounding the impeller and part of the impeller shaft. Draft tube is used to ensure a specific flow pattern to be set up in the fluid system for effective mixing. The size and location of the draft tube shall be determined based on the mechanical and mixing performance characteristics of the particular mixing application. Draft tubes are normally used in conjunction with axial flow impellers.

5.6 *Impellers*

5.6.1 Essentially most agitating operations may be effected with any type of impellers. Use of an impeller which is not best for a particular duty may result in high power consumption or be slow to achieve the required results. For equipment of low cost, power consumption and efficiency are often of secondary importance provided the required effect is produced, and in such cases choice of best impeller is not critical. Problems which are likely to require much power or equipment, or to be specially difficult or critical for any reason should be investigated on an appropriate experimental scale and are to be scaled up (*see* **7**).

5.6.2 *Type of impellers* — The impellers are classified into the following types:

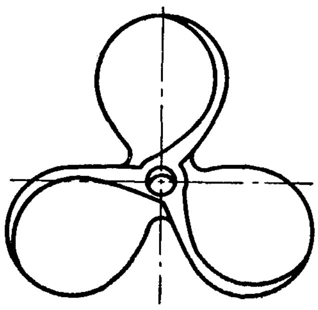
a) *Propellers* — Propellers are high speed impellers of the axial flow type. Marine type of impellers are most common in use and their shapes and contours vary widely.

b) *Turbines* — This type of impellers cover a wide variety of impellers which have nothing in common in regard to design, direction of discharge or character of flow. Impellers of this type which are in common use are flat blade, disc and blade, pitched blade, curved blade, tilted blade and shrouded types.

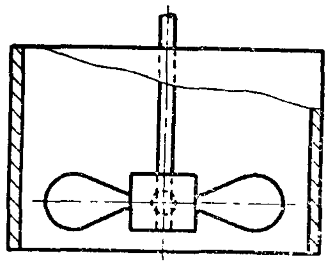
c) *Paddles* — The common types of impellers in this category are flat, paddle, anchor, plate, gate and helix.

d) *High shear impellers* — High shear impellers may be briefly characterized as low flow high velocity impellers suitable for application like emulsification and homogenization.

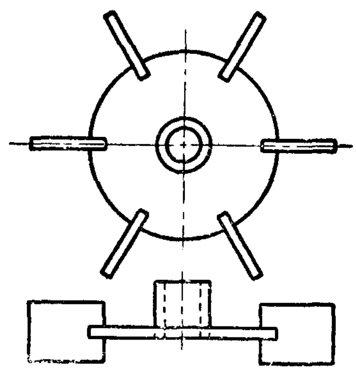
5.6.3 Some of the impellers in common use are shown in Fig. 2. The general description of these impellers and their applications are given in Table 2.



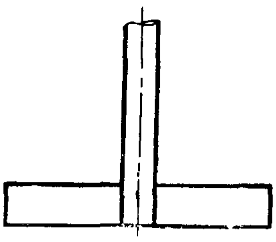
2A Propeller



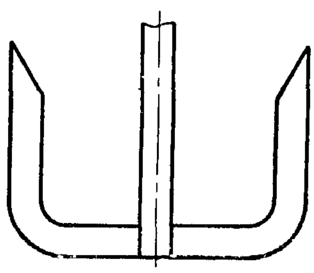
2B Propeller with Draft Tube



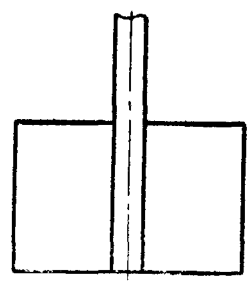
2C Disc with Blades (Turbine)



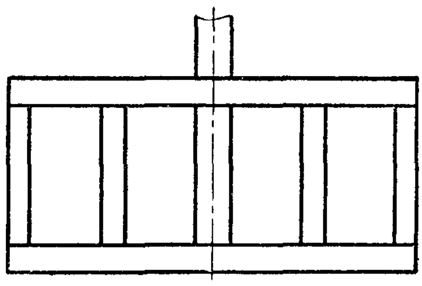
2D Flat Paddle



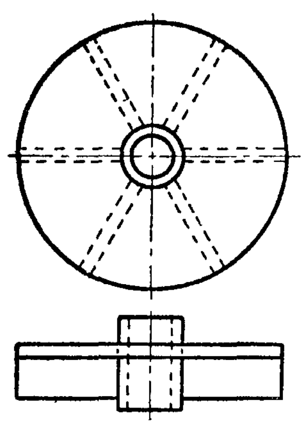
2E Anchor



2F Plate Paddle



2G Gate



2H Vaned Disc (Turbine)

FIG. 2 TYPES OF IMPELLERS

TABLE 2 IMPELLERS IN COMMON USE

(*Clause* 5.6.3)

Type of Impeller	Description	Application
(1)	(2)	(3)
Propeller	Wide variety in form, possible form simple twisted arms to properly formed marine propellers. No standardization of pitch or number of blades between manufacturers. Marine type propellers are usually less than 1/4th of the vessel diameter.	Basically high speed agitator but operates over wide speed range. Mass flow is vertical and little circumferential. Economical on power. Suitable for duties where agitation is not very intense and unsuitable for high viscosities. Much used for relatively small scale blending operations.
Propeller with draft tube	Propeller fitted below or just inside the lower end of draft tube. Baffles may be fitted in the draft tube. Top of draft tube may be just above or below the standing liquid level.	Applications similar to those of simple propeller, but more positive turnover of liquid and its flow through the impeller is ensured which is advantageous in wetting out some solids and mixing some immiscible liquids. By suitable location of the top level of the draft tube, a pouring action which will drown floating solids is achieved.
Turbine	Flat disc with blades attached to periphery. Similar effects are produced with the same number of blades directly attached to a boss. Overall diameter of the impeller is usually 1/3rd of the vessel diameter.	Generally moderately fast running agitator and versatile. Particularly suitable for high intensities of agitation and high power inputs. Recommended for applications where gas dispersion combined with intense agitation is required.
Flat paddle	Single flat blade (two arms) usually about 2/3rd of the vessel diameter.	Generally low speed agitator capable of producing high intensities of agitation, especially when baffled.
Anchor	Agitator following closely the contour of the vessel normally with a clearance of 25 mm to 40 mm between impeller and vessel wall.	A large low speed agitator, useful where the wall film must be disturbed like in heat transfer to viscous liquids from jacket, or where build up of solids on the wall is likely, as in crystallization. At low speeds has a very gentle action and will prevent caking in the bottom of vessel without vigorous agitation elsewhere. Widely used in enamelled equipment.
Plate	A square or rectangular plate bisected by the shaft on which it is mounted. Length usually 1/3rd to 1/2 of that of vessel diameter.	Similar applications to those of flat paddle, but allows more clearance for heating coils, fittings, etc, in the vessel. Where the depth of the plate is large relative to liquid depth, vertical movement of the liquid is less than that of a paddle of equivalent power.
Gate	An assembly of horizontal and vertical strips sometimes with diagonal bracing. Normally of length approaching vessel diameter and of depth about 1/2 to 3/4th of overall length.	A large low speed agitator of similar applications to those of anchor, but normally allows more clearance for coils and internal fittings in the vessel. It does not have the close sweeping effect of an anchor on the vessel walls and boss.
Vaned disc	A circular disc, usually 1/6th to 1/2 of vessel diameter with radial vanes 1/6th to 1/24th of disc diameter deep on its underside.	A small or moderately sized high speed agitator, limited usually to gas dispersion. The gas is fed under the centre of the disc. The power consumption without gas flow will be much higher than when gas is on, and drive should be adequate to cover the gasless condition.

6. Guidelines for the Selection of Impeller and Scaling Up

6.1 *Agitation* — In all applications of agitation, the primary effects are concerned with one or more of the following three physical processes:

a) Mass transfer;

b) Heat transfer; and

c) Dispersion of solids, liquids or gases.

Agitation does not directly affect the chemical reaction, if involved, but the rate of chemical reaction taking place may be influenced by one or more of the above primary effects. The factors which influence the rate and degree of mixing as well as the efficiency are classified as follows:

a) *Characteristics of impeller* — Its shape, speed, dimensions, and position in the vessel.

b) *Physical properties of the fluids* — Densities, viscosities and physical states.

c) *Vessel configuration* — Shape and dimensions of the containing vessel and of any fittings which may be immersed in the fluid.

6.2 Although agitation is concerned with obtaining the primary effects mentioned above, it is not easy to specify the exact circumstances needed to achieve them efficiently. This is because of the fact that the physical properties of the materials being processed are themselves the main factors which determine the choice of impeller and because these physical properties of the fluids vary widely.

6.3 All agitators impart kinetic energy to the fluids in the form of general mass flow and turbulence. Different mixing problems require different proportions of these two forms of kinetic energy at different levels of intensity. Characteristics required for various operations are given in Table 3.

TABLE 3 CHARACTERISTICS REQUIRED FOR SPECIFIC OPERATIONS

Duty	Mass Flow		Turbulence	Recommended Basis for 'Scaling-Up'
	Direction	Quantity		
(1)	(2)	(3)	(4)	(5)
Heat transfer:				
a) to jacket	Circumferential	Large	Low	Constant tip speed
b) to coil	Circumferential and little vertical	Large	Low	
Suspending solids:				
a) Light solids	Vertical	Small	Low	Constant tip speed
b) Medium solids	Vertical	Moderate	Moderate	
c) Heavy solids	Vertical	Large	Moderate or high	
Blending miscible liquids:				
a) Thin liquids	Vertical and little circumferential	Small	Moderate	Constant tip speed
b) Medium liquids	Vertical and little circumferential	Small	Moderate	
c) Viscous liquids	Vertical and little circumferential	Moderate	Moderate	
Mixing immiscible liquids:				
a) Thin liquids	Vertical	Moderate	High	Constant power per unit volume
b) Medium liquids	Vertical	Moderate	High	
c) Viscous liquids	Vertical	Small	High	
Emulsifying liquid mixtures:				
a) Thin liquids	Vertical	Large	High to very high	Constant power per unit volume
b) Medium liquids	Vertical	Large	High	
c) Viscous liquids	Vertical	Moderate	High	
Dispersing gases in liquids	Vertical	Large	High	Constant power per unit volume
Mixing pastes	Vertical and circumferential	Moderate	Moderate	Constant power per unit volume
Dispersing agglomerated solids	Vertical and circumferential	Large	Moderate or high	Constant power per unit volume

6.4 General Considerations for Selection of Impellers

6.4.1 The following considerations shall be borne in mind for the power selection of the impeller.

6.4.1.1 *Baffles* — Baffles have the effect of reducing mass flow and increasing turbulence. The formation of vortex is prevented as circumferential flow is suppressed. They are useful where the application requires high turbulence and capable of absorbing high power at relatively low speeds of rotation.

6.4.1.2 *Speed of rotation* — The tip speeds of all impellers are nearly same for the same agitating effects except in the case of propellers and anchors. Consequently, for a given effect, smaller agitator needs to be run at higher speeds and if small agitators are desired the effects of higher speed on erosion, bearing wear, gland difficulties, vibration and allied effects should be tolerated.

6.4.1.3 *Impeller size* — For the same vessel a large agitator operating at low speed products relatively more mass flow and less turbulence than a smaller but geometrically similar agitator which operates at high speeds and transmits the same power.

6.4.1.4 *Number of impellers* — Large filling ratios are not recommended but where used should in general have one impeller for each vessel diameter of liquid depth.

6.4.1.5 *Power and viscosity* — Power level required increased with viscosity of liquid for the same mixing effect.

6.4.1.6 *Impeller speed and viscosity* — In general it is better to use large impellers at lower speeds as viscosity increases.

6.4.1.7 *Immiscible liquids* — In agitating immiscible liquids initially in two layers, the impeller must be kept near the interface.

6.4.1.8 *Gas dispersion* — Gases to be dispersed in liquids by mechanical agitation should be fed from underneath the centre of the impeller.

6.5 *Selection of Impeller Type* — The specific characteristics of commonly used impellers with and without baffles are described in Table 4. Having selected the required conditions for a specific operation from Table 3, the suitable impeller to achieve these conditions may be identified from Table 4.

6.5.1 *Practical limitations of impellers* — The following practical limitations regarding impellers should not be overlooked in selection and design of impellers:

a) It is difficult to construct anchors to operate at high speeds (that is greater than a tip speed of 300 metres per minute) or to make anchors for vessels exceed 2 800 mm diameter.

b) Gate type impellers are not usually desirable for mixing in vessels of less than 1 800 mm diameter. The extra application compared with an anchor or flat paddle is not worthwhile.

c) Propellers and other high speed impellers should not be used in high viscosity liquids for general agitation, since their effect rapidly falls with distance from the impeller and causing excessive power loss.

d) The various impellers referred below generally should not be used with viscosities exceeding the value shown against them:

Flat paddle	1×10^6 cP
Turbine	2×10^5 cP
Propeller	3×10^3 cP
Plate	5×10^5 cP
Vaned disc	5×10^3 cP
Anchor	7×10^5 cP
Gate	1×10^5 cP

7. Scaling Up

7.1 For scaling up the results obtained on experimental basis, the same liquid should be used in the small and large scale vessels and also the vessels and impellers should be geometrically similar. The two typical bases used for scaling up the experimental results are:

a) Constant impeller tip speed, and

b) Constant power input per unit volume.

TABLE 4 CHOICE OF IMPELLERS

(*Clause* 6.5)

Direction of Mass Flow	Baffles	Impeller	Turbulence	Mass Flow	Remarks
(1)	(2)	(3)	(4)	(5)	(6)
Vertical	Yes	Paddle	Moderate High Very high	Small Moderate to large Very large	
		Turbine	Moderate High Very high	Small Moderate to large Very large	
		Propeller (with or without draft tube)	High	Moderate to large	
		Plate	Moderate High Very high	Small Moderate to large Large	
		Vaned disc	Moderate High Very high	Small to moderate Moderate to large Large	Mass flow increases with increase in impeller tip speed
Vertical and little circumferential	No	Propeller	Low Moderate	Small to moderate Moderate to large	
		Propeller and draft tube	Low Moderate	Moderate Moderate to large	
Vertical and circumferential	No	Paddle	Low Moderate	Small Moderate to very large	
		Turbine	Low Moderate	Small Moderate to large	
		Plate	Low Moderate	Small Moderate to very large	
Circumferential	No	Anchor	Low Moderate	Small to moderate Large to very large	
		Gate	Low Moderate	Small to moderate Moderate to very large	

It is considered that no general choice may be made between the above two bases of scaling up and that each type of duty should be dealt with individually. The duties, however, may be divided between these two methods on the following general principles:

a) Where the duty demands a similar flow pattern with similar velocities, constant tip speed is recommended, and

b) Where the duty requires vigorous liquid movement, constant power input per unit volume is recommended.

7.2 If the category cannot be decided, it is safer to use the basis of constant power per unit volume.

7.3 For specific operations, the recommended basis for scaling up is given in Table 3.

8. Guidelines on Power Assessment

8.1 The power required for agitation shall be considered mainly based on the following two aspects:

a) The power required under normal operating conditions, and

b) The power need to cover start-up conditions and peak loads.

8.2 The power required under normal operating conditions constitutes the sum of:

a) The power required by the impeller under normal operating conditions,

b) Gland losses and

c) Losses in the driving system.

8.2.1 *Power required by the impeller under normal operating conditions* — The power required by the impeller may be computed based on the physical properties of fluids involved, size and shape of vessel, type, size and speed of impeller and nature of fittings involved in the vessel. The actual method of computation of power required by the impeller is not covered by this standard.

8.2.2 *Gland losses* — It is found in practice that the power loss in gland varies from less than 0·3 kW for the small impeller shafts up to 3 kW for the larger. Where no relevant experience is available, as a rough approximation the gland losses may be taken as 10 percent of the agitator power consumption, or 0·3 kW, whichever is greater.

8.2.3 *Drive loss* — The power loss in a gear box is a function of the rated power capacity of the gear box. Operation at low loads causes a considerable drop in efficiency due to lower working temperature. It is, therefore, usual to allow 20 percent of the maximum input rating as the gear box and V-belt drive loss. Where no gear box is used 5 percent of the horse power required by the agitator may be taken as losses in drive.

8.3 *Power Needed to Cover up, Start up and Peak Loads* — Factors like the presence of cold lubricant in the gear box at the time of starting, the possibility of solid settling out, addition of new materials into the vessels during operation which exists only during starting or during unusual operation conditions may need additional power from the motor to cope up. Hence, the calculated power needed under normal operating conditions shall be suitably augmented while arriving at the motor capacity to ensure that the motor is capable of dealing with the heaviest loads likely to occur during start up and unusual operating conditions in practice.

9. Drive and Bearing Arrangements

9.1 *Drive* — All impellers should be independently driven by a standard electric motor of the vertically or horizontally mounted type. For speed reduction, a V-belt drive from the motor to the gear box is recommended to enable standard gear box ratios to be used, and to give some degree of flexibility in impeller speeds after installation. For impellers operating at high speeds the required speed reduction may be obtained by a V-belt drive alone. Where the agitator shaft passes through a stuffing box or a seal, the drive should be mounted on a rigid body fixed to the top of the vessel to minimize differential movement. Wherever V-belt drive is used the driving motor itself should be mounted on slide rails so that adjustments may be made to the V-belt drive for small speed adjustments. Alternatively gear boxes fitted with a hinged-motor mounting on top for this purpose shall be used.

9.2 *Gear Box* — The size of the gear box should be at least equivalent to the rating of the motor being used and should be 24 hour rating type.

9.3 *Couplings and Bearings* — The economical method of supporting the impeller shaft would be to use a gear box carrying bearing to accommodate the bending and thrust loads of the impeller shafts, the impeller shaft being rigidly coupled to the output shaft of the gear box. This arrangement is quite suitable for use with shaft passing through stuffing box designed for low pressure duties or where a steady bearing is fitted inside the vessel. However, for installations with long impeller shafts, or where the load is such that bearings are required on the shaft, or where deep stuffing boxes have to be used like in high pressure agitator vessels like auto-claves, it is preferable to fit bearings on the shaft immediately above the stuffing box and a steady bearing inside the vessel below the stuffing box. In such cases the impeller shaft shall be connected to the gear box by a flexible coupling.

Coupling between the gear output and impeller shafts may be of any conventional design. For corrosive service it is preferable to arrange couplings between drive and impeller shaft, outside the vessel, even though this entails longer shafts and may necessitate additional bearings.

9.4 *Glands and Bushes* — Gland should be easily accessible for removal of packing and repacking and where lantern rings are provided, care should be taken to see that they do not operate as a bearing. In high temperature service the gland should be raised sufficiently high above the vessel for ease of cooling. Normally no bearing bush is necessary for pressure application up to 20 kg/cm^2 and where the impeller shaft is robust with its bearings fitted near enough to the stuffing box.

For high pressure service or where particularly high standard of performance is demanded from the gland, a bush in the base of the stuffing box is desirable.

Mechanical seals may be used in place of the glands in the agitator vessels. However, when mechanical seals are employed correct alignment and rigidity of the shaft shall be ensured for the proper functioning of the seals.

10. Mechanical Design

10.1 Design of vessels, flanges and others shall be made in accordance with IS : 2825-1969 'Code for unfired pressure vessels'.

10.2 *Guidelines for the Design of Agitator Shaft* — The stresses that would be included in the agitator shafts are considerably higher than the design torque at normal operating conditions may induce due to various reasons mentioned below. To avoid functional damage and to ensure satisfactory service, the shaft should be designed based on the criteria given below, using the appropriate design formulae.

10.2.1 *Starting torque* — During starting conventional types of electric motors, the starting torque is more than the full load rated motor torque. To avoid undue distortion in the shaft due to starting torque, the shaft should be designed to resist 2½ times the motor rated torque as pure torque without exceeding the safe working stress of the shaft material.

10.2.2 *Stalling of impeller* — There is also a possibility of the impeller being checked in situations like addition of materials into the vessel by tipping bags. In such stalled conditions the impeller shaft should not fail before the overload protection of the motor operated. A method of design, found successful, is to make the shaft sufficiently strong to withstand, without exceeding the yield stress of the material, the stresses which would be set up if the agitator blades were jammed at a point 75 percent of its length from the shaft. The torque prevailing under stalled conditions may be taken as 1·5 times and 2·5 times the motor rated torque for shafts of light duty and heavy duty respectively. Low speed impellers, well clear off from vessel walls or baffles, and in vessels where no solids are charged or precipitated and where the application needs less power input per unit volume are called light duty applications and the rest are high duty applications.

10.2.3 *Fouling in stalled conditions* — The shafts should be designed so as to be rigid enough and should not deflect to an extent as to cause fouling of the vessel walls, baffles or any other internal fittings when jammed.

10.2.4 *Balancing* — The tolerance on straightness of shafts, symmetry of the impeller and general accuracy need to be progressively tightened as speeds and power increase. Static balancing is recommended for shaft and impeller assemblies over 2·5 metres long and operating above 100 rpm, and dynamic balancing for shaft and impeller assemblies over 3·7 metres long and operating above 150 rpm.

10.2.5 *Critical speed* — The shaft, normally should not run within 30 percent of its critical speed, but when dynamically balanced this limit may be reduced to 15 percent.

10.2.6 *Shaft sizes* — To avoid the use of irrational and innumerable shaft sizes and to avoid difficulties in procuring associated parts like bearings, bushes and seals, shaft diameters should be in accordance with IS : 3132-1965 'Recommendation for shaft diameters for chemical equipment.'

EXPLANATORY NOTE

Agitator equipments are widely used in chemical and process industries for operations like blending, dissolution, precipitation, extraction and dispersion. The subject of mixing has been one of the most difficult of the unit operations of chemical engineering to submit to scientific analysis. Moreover, there is little published information concerning the selection of impellers for economical operation and power calculations. Due to the facts mentioned above the scope of this standard has been limited mostly to recommendatory nature.

This Code gives the various features of the agitator equipment and gives guidance on the selection of impellers, and other design features.

The recommended capacities of vessels given in this Code are based on the R5 and R10 series of preferred numbers in accordance with IS : 1076-1967 'Preferred numbers (*first revision*)'.

In the aspect of mechanical design, only guidelines for the impeller shaft are given. For the design of vessels, flanges and others, Indian Standard Code for unfired pressure vessels (IS : 2825-1969) shall apply.

In the preparation of this standard considerable assistance has been derived from the Handbook No. 9 of Engineering Equipment Users' Association, London.